

## Chemistry 553

### Problem set 5

Due: 11 March 2011

From your text,

1. 14.1
2. 14.6
3. 15.3 use a graphics package
4. 16.2
5. 16.5
6. 16.21
7. 25.3
8. 25.10
9. a few more to come

Problem set 5

1. 14.1

$$a) \left( \frac{\partial \ln P}{\partial T} \right) = \frac{\Delta H}{RT^2} \Rightarrow \left( \frac{\Delta \ln P}{\Delta T} \right) = \frac{\ln(760/23)}{373 - 300}$$

$$\Delta H \sim RT^2 (0.048) = (8.315 \frac{J}{K})(373)(0.048) \sim 55.4 \text{ kJ}$$

~~~ 118 kJ~~  
mole

$$\text{or } \frac{\partial \ln P}{\partial (1/T)} = -\frac{\Delta H}{R} \therefore \frac{\Delta \ln P}{\Delta (1/T)} = 44.6 \text{ kJ/mole}$$

$$b) \ln(P_2/P_1) = \frac{ZW_{AA}}{2R} \left( \frac{1}{T_2} - \frac{1}{T_1} \right) \quad \text{lattice model}$$

$$\frac{\Delta H}{R} = -\frac{ZW_{AA}}{2R}, \text{ since } \frac{\partial \ln P}{\partial (1/T)} = \frac{ZW_{AA}}{2R}$$

$$\text{and } W_{AA} = \frac{2}{Z} \Delta H = \frac{1}{2} \Delta H(L \rightarrow G) = 22.3 \text{ kJ/mole}$$

2. 14.6

$$P = P_{int}^0 \exp(ZW_{AA}/2RT)$$

$$\text{but } \Delta H_{vap} = -ZW_{AA}/2 \quad \text{given above}$$

$$P = P_0 \exp(-\Delta H_{vap}/RT) \Rightarrow \text{if the } P_0\text{'s are the same then}$$

$$\frac{\Delta H_{vap}}{T} \Big|_{\text{fluid a}} = \frac{\Delta H_{vap}}{T} \Big|_{\text{fluid b}}$$

$$\text{and } \frac{T_b}{T_a} = \frac{\Delta H_{vap,b}}{\Delta H_{vap,a}} = \frac{15 \text{ kcal}}{10 \text{ kcal}} = \frac{T}{300}$$

$$T = 450 \text{ K.}$$

3. 15.3

```
> mu := ln(x) + chi*(1-x)^2;
```

$$\mu := \ln(x) + \chi(1-x)^2$$

```
> mu_0 := subs(chi=0,mu);
```

```
> mu_2 := subs(chi=2,mu);
```

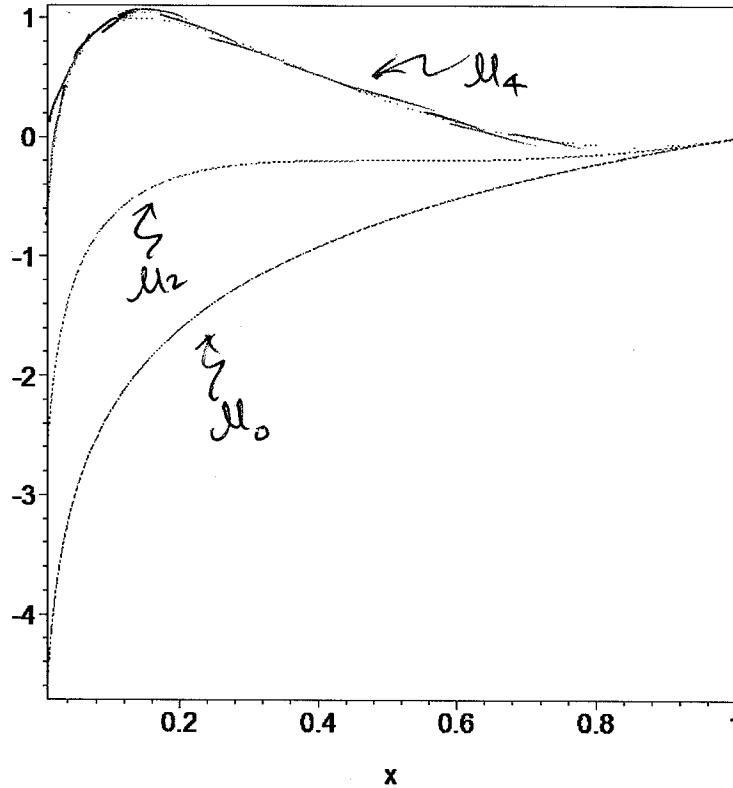
```
> mu_4 := subs(chi=4,mu);
```

$$\mu_0 := \ln(x)$$

$$\mu_2 := \ln(x) + 2(1-x)^2$$

$$\mu_4 := \ln(x) + 4(1-x)^2$$

```
> plot([mu_0,mu_2,mu_4],x=0.01..1,axes=boxed);
```



```
>
```

3. 15.3 Plot  $\mu(x)$ ,

$$\beta \mu(x) = \ln x_A + \frac{zW_{AA}}{2RT} + \chi_{AB}(1-x_A)^2$$

$\chi_{AB} = 0, \chi_{AB} = 2, 4$  (see enclosed plot).

4. 16.2

$$P_{\text{vapor pressure of } N_2} = k_H X_{N_2}$$

$\approx$

86,000 atm

As we compress water, <sup>the</sup> vapor pressure of the  $N_2$  also increases.

$$P = 1 \text{ atm} + \frac{d(\text{feet})}{33 \text{ ft/atm}}$$

air is 78%  $N_2$

$$X_{N_2} = \frac{0.78}{86 \times 10^3} \left\{ 1 + \frac{d(\text{ft})}{33} \right\}$$

5. T-dependence of the Henry's law const.

$$P_B = X_B P_B^0 \exp(\chi_{AB}(1-X_B)^2)$$

$$\begin{aligned} \chi_{AB} &= z \left\{ W_{AB} - \frac{1}{2}(W_{AA} + W_{BB}) \right\} / R_B T \\ &= z \Delta W / R_B T \end{aligned}$$

Henry's law is the limit of  $X_B \rightarrow 0$

$$P_B = k_H X_B$$

$$k_H = k_H(T) + \Delta T \left( \frac{\partial k_H}{\partial T} \right) = k_H(T + \Delta T)$$

$$\frac{\partial}{\partial T} P_B^0 \exp(z \Delta W / RT) = - \frac{z \Delta W}{RT^2} P_B^0$$

$$\therefore \left( \frac{\partial P_B}{\partial T} \right) = - \frac{z \Delta W}{RT^2} P_B(T)$$

6. 16.21 From the figure,  $\chi \approx 2$ , so that

$$\chi_{AB} = 2 = z \Delta W / RT$$

$\uparrow$   
3, and  $\Delta W \sim \frac{1}{3} RT$

a)  $\Delta W / \text{mole} \sim \frac{1}{3} RT \sim \frac{300}{3} R = 100 R \approx 8.3 \text{ kJ}$

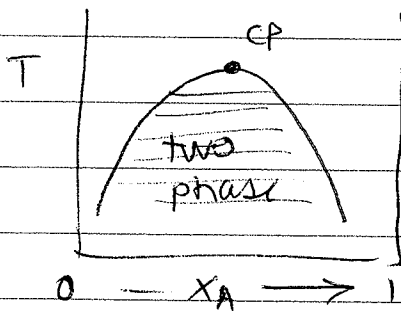
b)  $\chi_{AB} \approx 2$

c)  $P_B = X_B P_B^0 \exp(\chi_{AB} (1 - X_B)^2)$

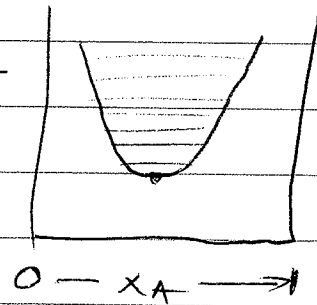
as  $X_B \rightarrow 1$ ,  $P_B \rightarrow X_B P_B^0$   
Raoult's law.

7. 25.3

Normally



when  $\chi$  increases with  $T$ , phase separation occurs  $\Leftrightarrow T > T_c$ .



8. 25.10

At compositions near the Azeotrope,

distillation will ~~not~~ always produce the pure mixture, i.e., can not be separated into pure components.